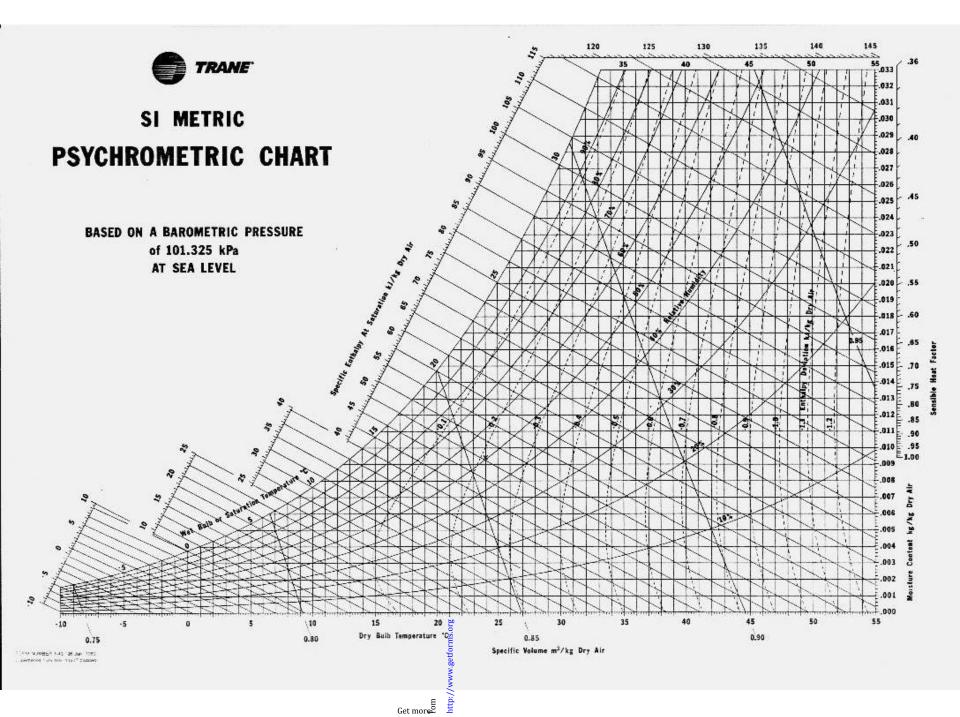
THE PSYCHROMETRIC CHART: Theory and Application

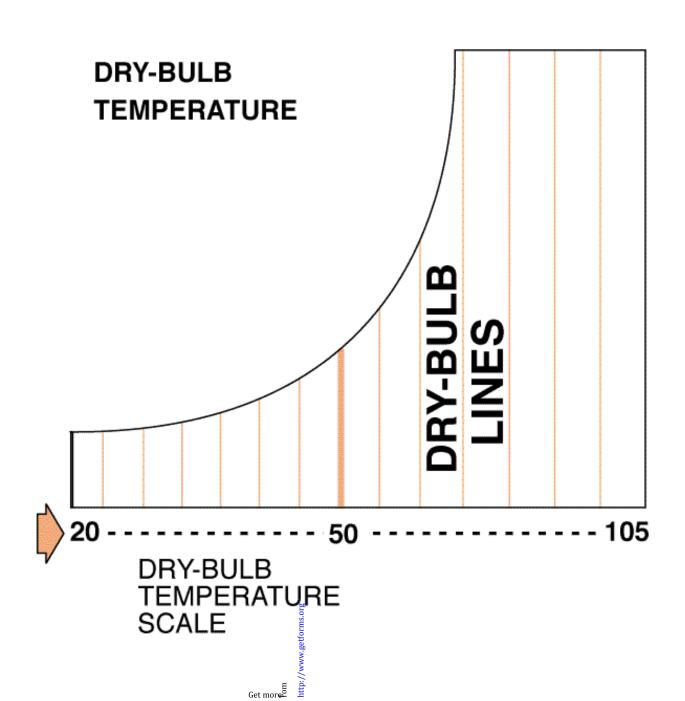
Perry Peralta

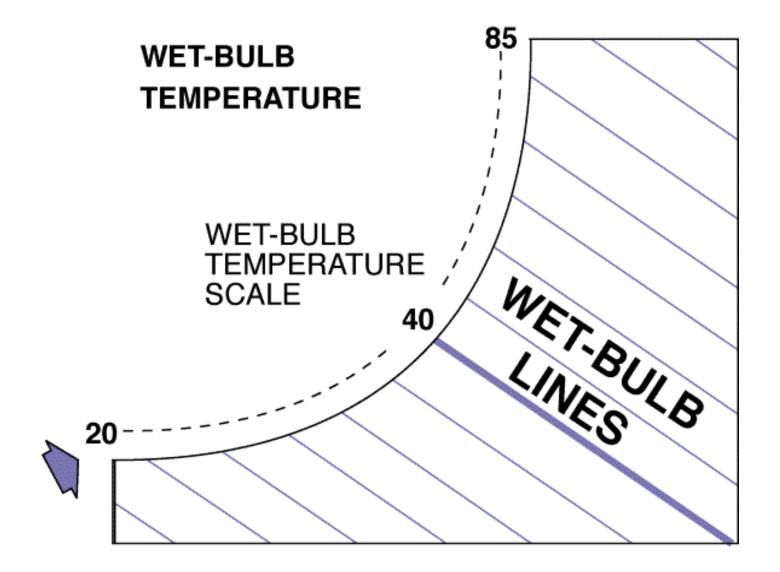
NC State University

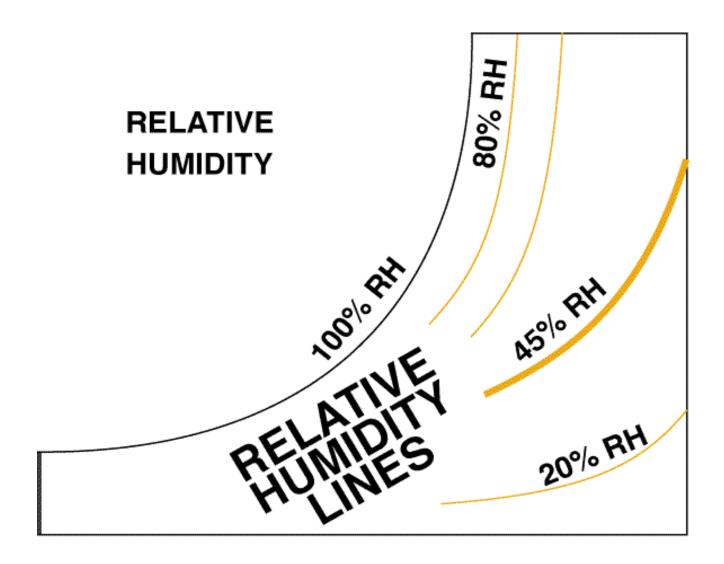
PSYCHROMETRIC CHART

- Identify parts of the chart
- Determine moist air properties
- Use chart to analyze processes involving moist air



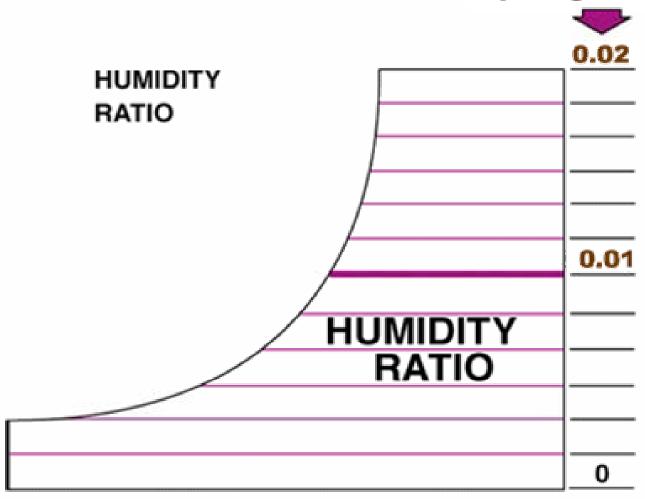


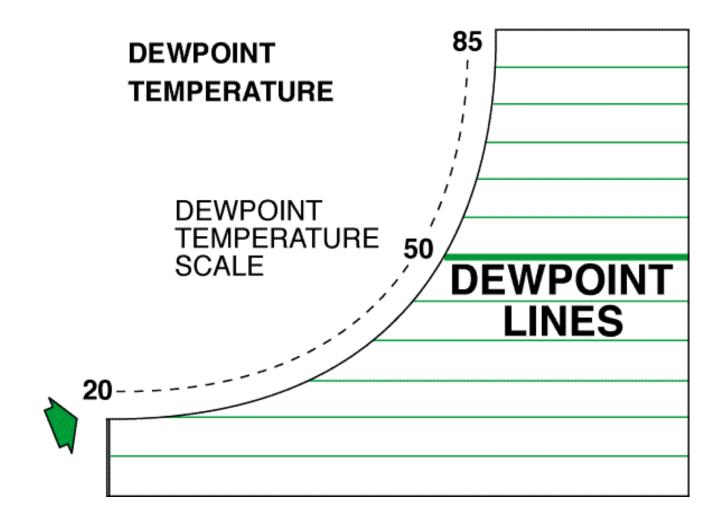


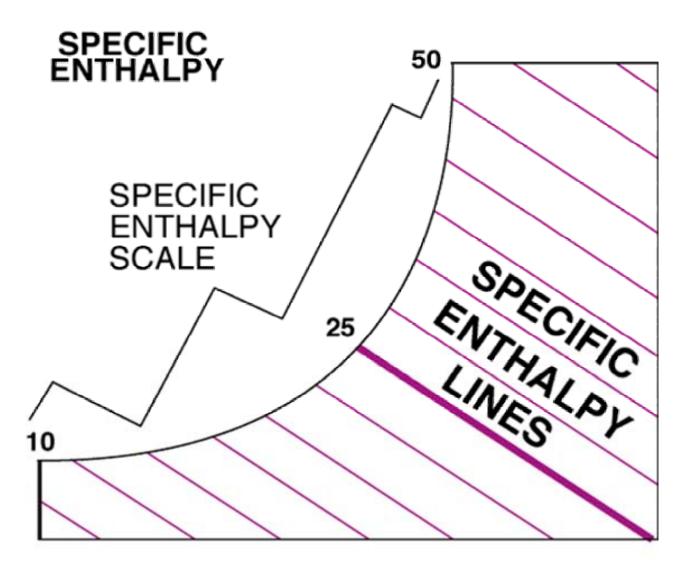


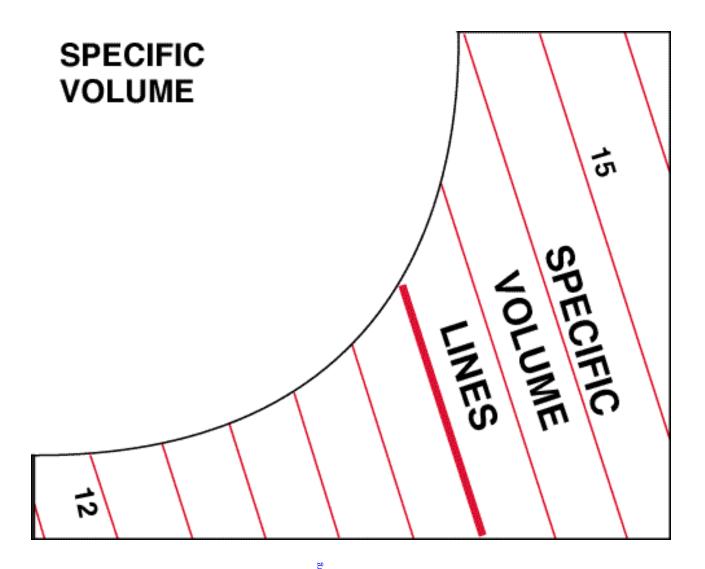
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Kg of moisture per kg of dry air









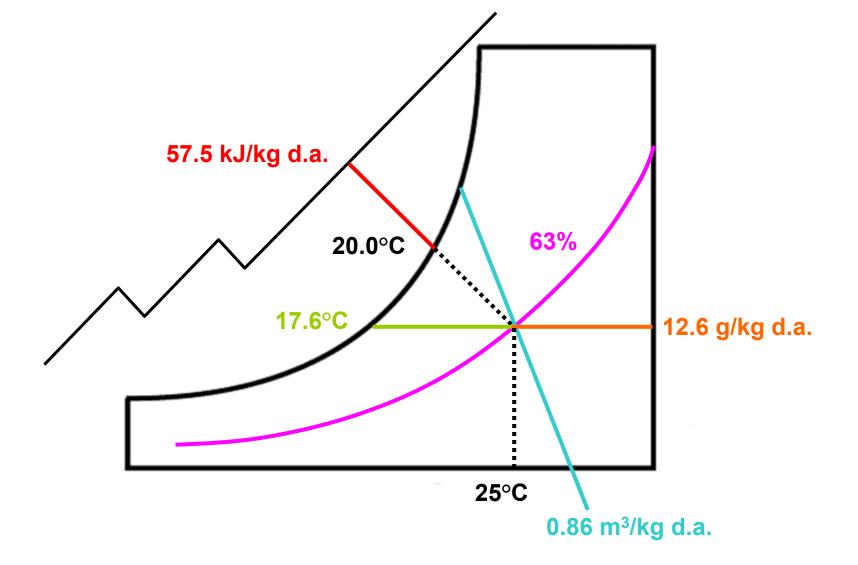
Psychrometric chart: Example 1

Given: $T = 25^{\circ}C$

 $T_w = 20$ °C

Required: (a) RH, (b) T_{dp}, (c) HR, (d) v, (e) h

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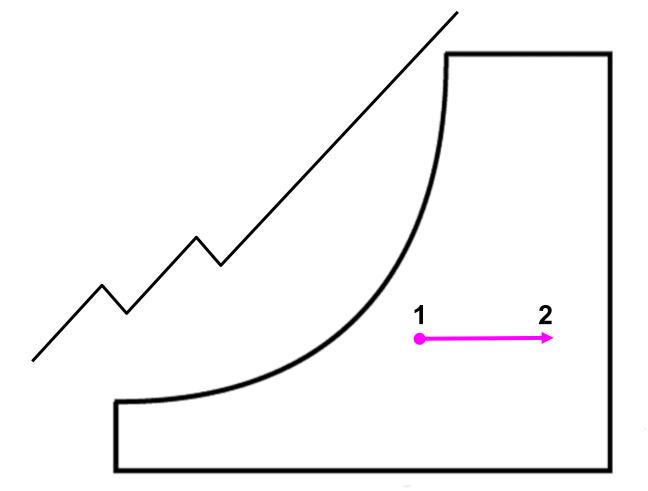
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PSYCHROMETRIC PROCESSES

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Sensible Heating or Cooling

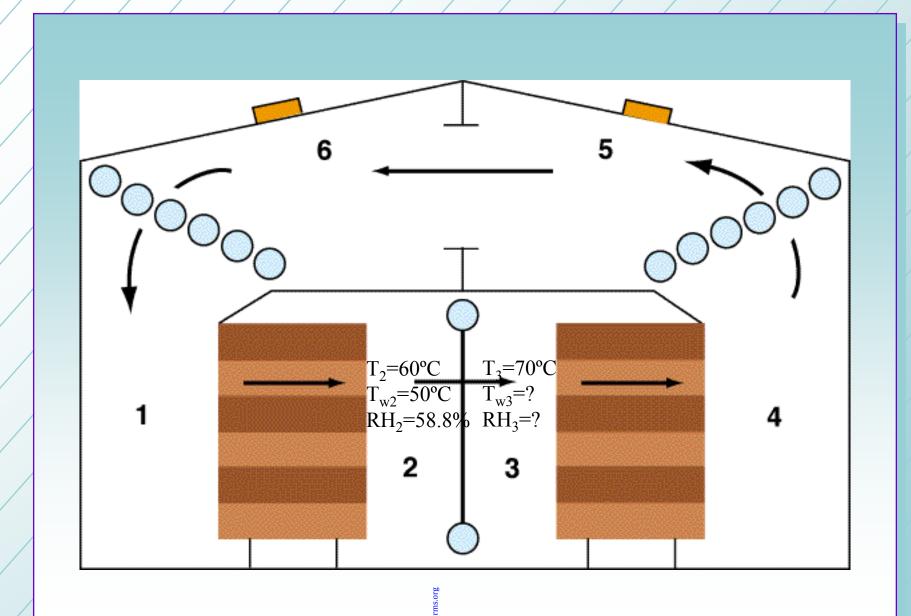
- a psychrometric process that involves the increase or decrease in the temperature of air without changing its humidity ratio
- Example: passing moist air over a room space heater and of kiln air over the heating coils

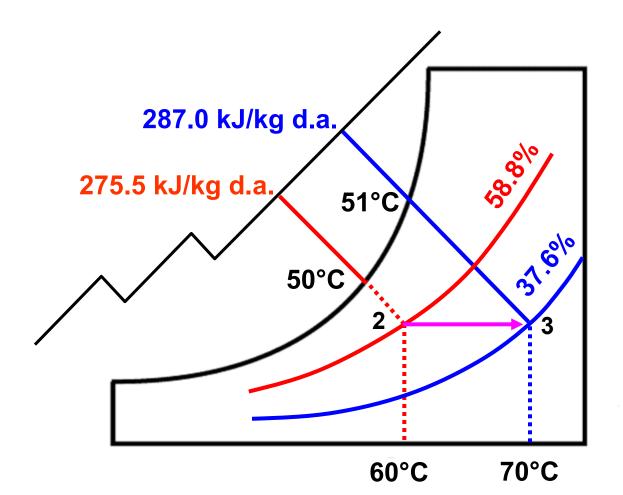


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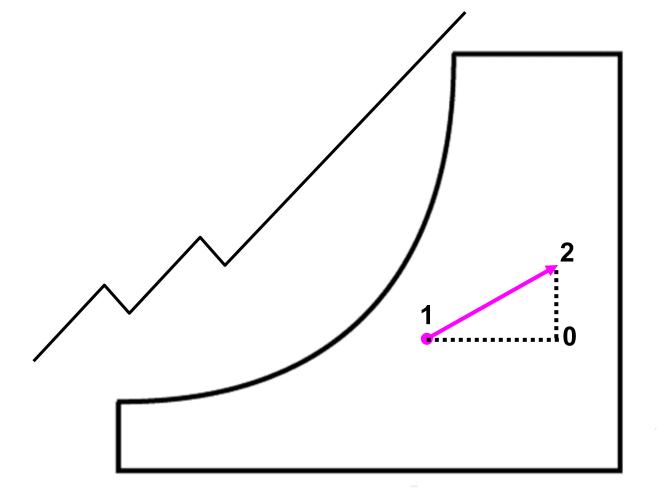
Sensible heating: Example 5





Heating and Humidifying

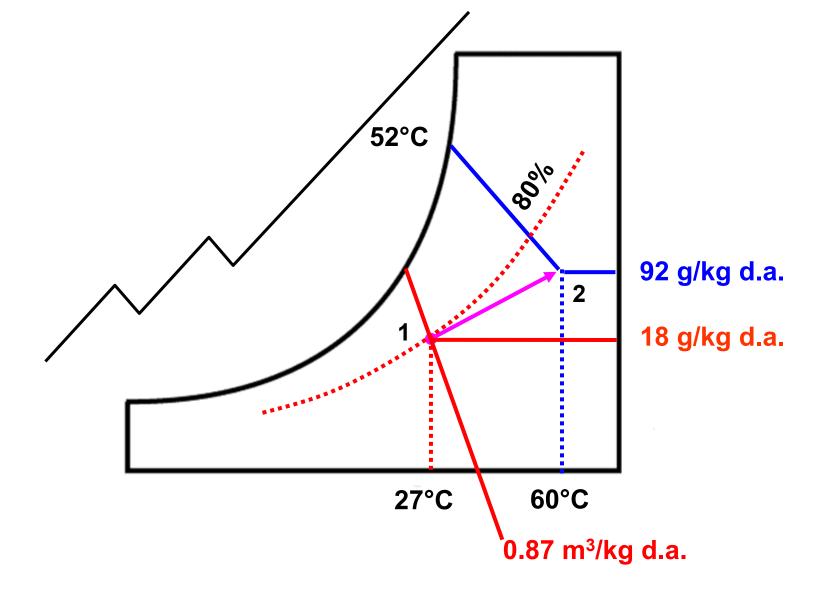
 a psychrometric process that involves the simultaneous increase in both the dry bulb temperature and humidity ratio of the air



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Heating and humidifying: Example 7

Two and a half cubic meters of lumber is being dried at 60°C dry bulb temperature and 52°C wet bulb temperature. The drying rate of the lumber is 12.5 kg of water per hour. If outside air is at 27°C dry bulb temperature and 80% relative humidity, how much outside air is needed per minute to carry away the evaporated moisture?



Heating and humidifying: Example 7

```
\Delta HR = (92.0 - 18.0) \text{ g/kg dry air}
= 74.0 g/kg dry air
```

```
w_{a1} = drying rate/\DeltaHR
= (12.5 kg/hour)/(0.074 kg/kg dry air)
= 168.9 kg dry air/hour
```

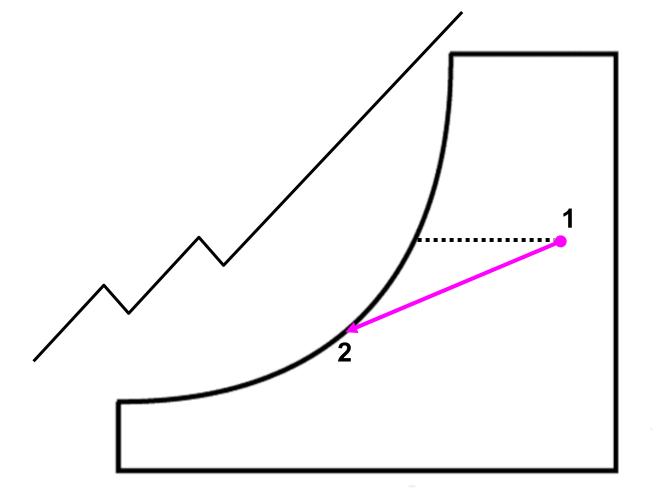
$$VF_1 = (w_{a1})(v_1)$$

= (168.9 kg dry air/hour)(0.87 m³/kg dry air)
= 147 m³/hour = 2.45 m³/minute

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Cooling and Dehumidifying

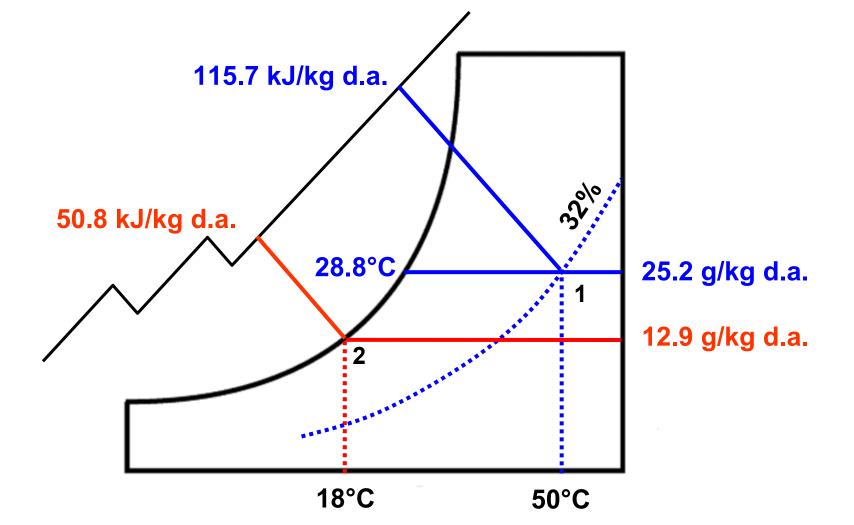
a psychrometric process that involves the removal of water from the air as the air temperature falls below the dewpoint temperature



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Cooling and dehumidifying: Example 9

Moist air at 50°C dry bulb temperature and 32% relative humidity enters the cooling coil of a dehumidification kiln heat pump system and is cooled to a temperature of 18°C. If the drying rate of 6 m³ of red oak lumber is 4 kg/hour, determine the kW of refrigeration required.



Cooling and dehumidifying: Example 9

$$\Delta$$
HR = (25.2 – 12.9) g water/kg dry air
= 12.3 g water/kg dry air

$$w_{a} = \frac{\text{drying rate}}{\Delta HR}$$

$$= \frac{4 \text{ kg water}}{0.0123 \text{ kg water}}$$

$$= \frac{0.0123 \text{ kg water}}{\text{kg dry air}}$$

Cet more

Cooling and dehumidifying: Example 9

$$\Delta h = (115.7 - 50.8) \text{ kJ/kg dry air}$$

= 64.9 kJ/kg dry air

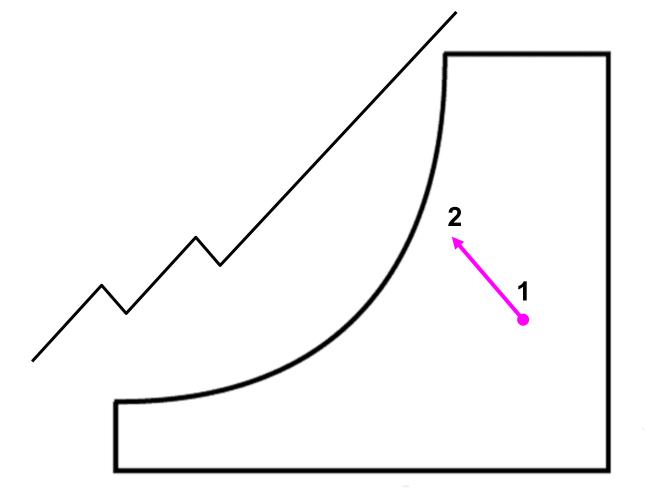
$$q = (\Delta h)(w_a)$$

$$= \left[64.9 \frac{kJ}{kg \text{ dry air}}\right] \left[325.2 \frac{kg \text{ dry air}}{h}\right]$$

$$= 21105.7 \frac{kJ}{h} = 5.9 \text{ kW}$$

Adiabatic or Evaporative Cooling

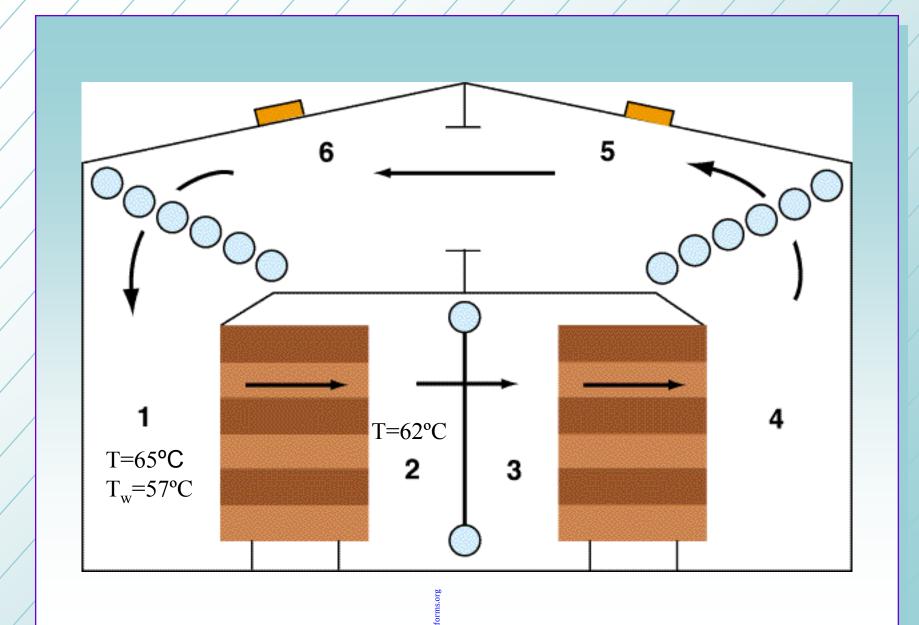
a psychrometric process that involves the cooling of air without heat loss or gain. Sensible heat lost by the air is converted to latent heat in the added water vapor



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Evaporative cooling: Example 10

Referring to Figure 21, air at state point 1 (65°C dry bulb temperature and 57°C wet bulb temperature) experiences a temperature drop of 3°C as it passes through the 1.2-m wide stack of lumber. Determine the properties of the air at state point 2 and compare them with those at state point 1. If the air is flowing at a rate of 2 meters per second, determine the drying rate assuming that the volume of the stack of 2.5-cm-thick lumber is 2.5 m³. The stack is 1.2 m wide x 3.6 m long, and the boards are separated by stickers 3.8 cm wide x 1.9 cm thick that are spaced 0.6 m apart.



Evaporative cooling: Example 10

Given: $T_1 = 65^{\circ}C$; $T_{w1} = 57^{\circ}C$

Adiabatic cooling to $T_2 = 62^{\circ}C$

Air flow rate = 2 m/s

Volume of lumber = 2.5 m^3

Board thickness = 2.5 cm

Stack dimensions: 1.2 m wide x 3.6 m long

Sticker dimensions: 3.8 cm wide x 1.9 cm thick

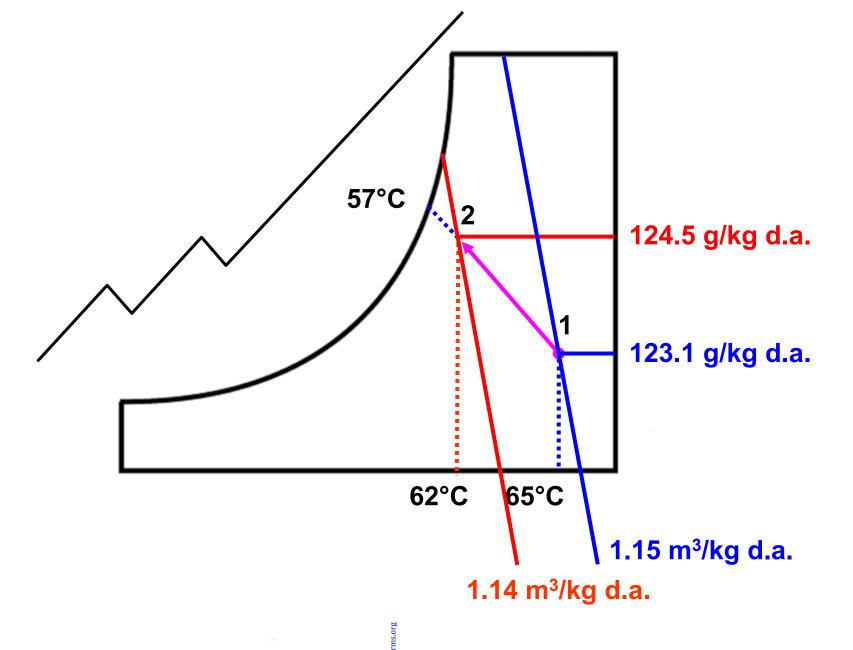
Sticker spacing = 0.6 m

Required: (a) Properties of the air at state point 2 relative to that at state point 1

(b) Drying rate

Solution:





Evaporative cooling: Example 10

(a) At state point 1:
$$T_1 = 65^{\circ}\text{C}$$

 $T_{w1} = 57^{\circ}\text{C}$
 $T_{dp1} = 56.3^{\circ}\text{C}$
 $RH_1 = 66.9\%$
 $HR_1 = 123.1 \text{ g/kg of dry air}$
 $v_1 = 1.15 \text{ m}^3/\text{kg of dry air}$
 $h_1 = 387.7 \text{ kJ/kg of dry air}$

At state point 2:
$$T_2 = 62^{\circ}\text{C}$$

 $T_{w2} = 57^{\circ}\text{C}$
 $T_{dp2} = 56.5^{\circ}\text{C}$
 $RH_2 = 77.3\%$
 $HR_2 = 124.5 \text{ g/kg of dry air}$
 $v_2 = 1.14 \text{ m}^3/\text{kg of dry air}$
 $h_2 = 387.7 \text{ kJ/kg of dry air}$

(b) Drying rate = $(\Delta HR)(w_a)$

$$\mathbf{w}_{a} = \frac{\mathbf{VF}}{\mathbf{v}_{2}}$$

$$VF = (A)(air flow rate)$$

$$A = \left(\frac{V}{P_1 P_w B_t}\right) \left(P_1 S_t - \frac{P_1 + S_s}{S_s} S_t S_w\right)$$

$$A = \left(\frac{2.5}{3.6*1.2*0.025}\right) \left(3.6*0.019 - \frac{3.6+0.6}{0.6}0.019*0.038\right)$$

$$A = 1.47 \text{ m}^2$$

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$$A = 1.47 \text{ m}^2$$

$$VF = (A)(air flow rate)$$

$$VF = (1.47 \text{ m}^3) (2 \frac{\text{m}}{\text{s}}) = 2.9 \frac{\text{m}^3}{\text{s}}$$

$$VF = 2.9 \frac{m^3}{s}$$

$$\mathbf{W}_{\mathbf{a}} = \frac{\mathbf{VF}}{\mathbf{V}_{\mathbf{2}}}$$

$$w_{a} = \frac{2.9 \frac{\text{m}^{3}}{\text{S}}}{1.14 \frac{\text{m}^{3}}{\text{kg dry air}}} = 2.6 \frac{\text{kg dry air}}{\text{S}}$$

$$w_a = 2.6 \frac{\text{kg dry air}}{\text{s}}$$

Drying rate =
$$(w_a)(\Delta HR)$$

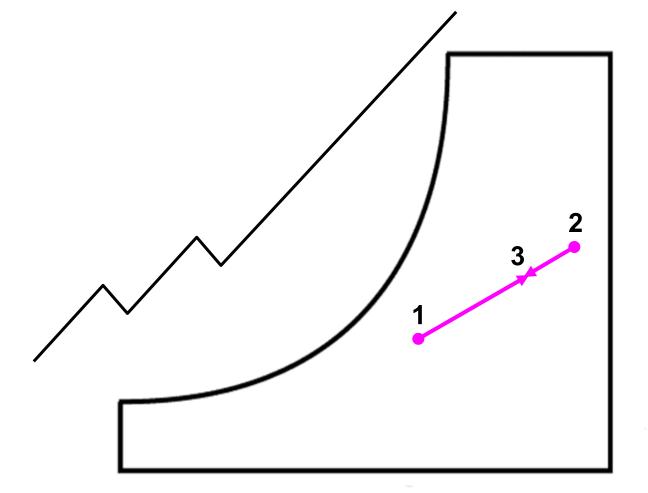
Drying rate =
$$\left(2.6 \frac{\text{kg dry air}}{\text{s}}\right) \left(1.4 \frac{\text{g}}{\text{kg dry air}}\right)$$

= $3.6 \frac{\text{g}}{\text{s}} = 13.0 \frac{\text{kg}}{\text{h}}$

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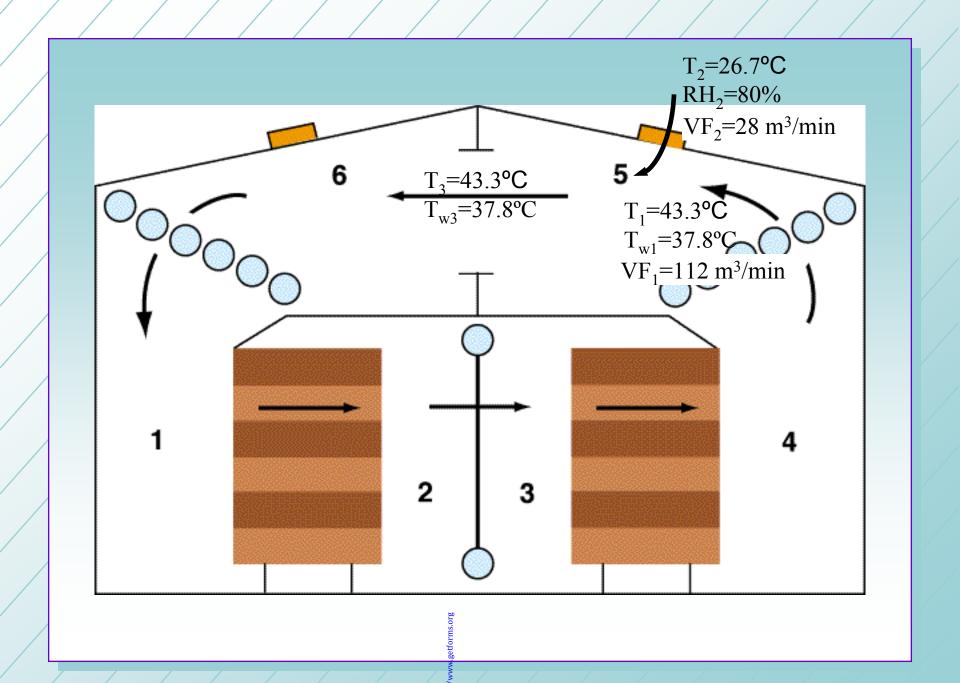
Adiabatic Mixing of Moist Air Stream

 A psychrometric process that involves no net heat loss or gain during the mixing of two air streams

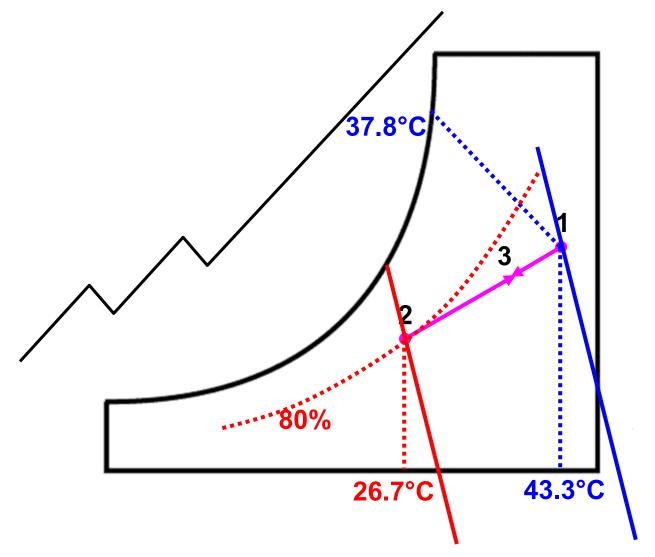


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0.87 m³/kg d.a. 0.95 m³/kg d.a.

$$\mathbf{w}_{a} = \frac{\mathbf{VF}}{\mathbf{V}}$$

$$w_{a1} = \frac{112 \frac{\text{m}^3}{\text{minute}}}{0.95 \frac{\text{m}^3}{\text{kg dry air}}} = 117.9 \frac{\text{kg dry air}}{\text{minute}}$$

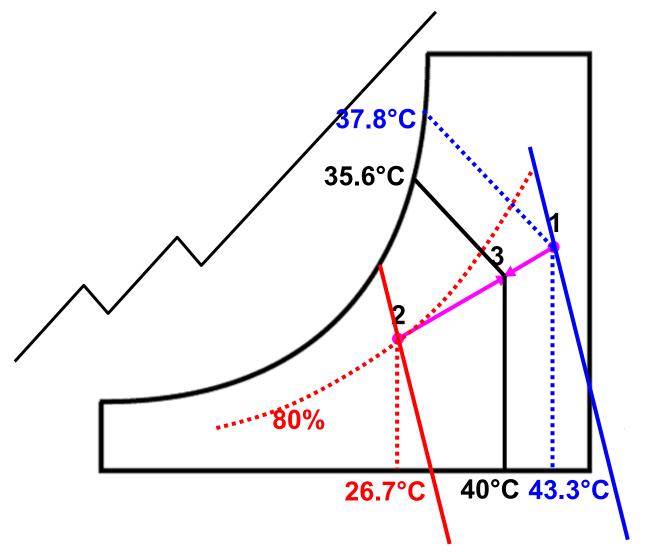
$$w_{a2} = \frac{28 \frac{\text{m}^3}{\text{minute}}}{0.87 \frac{\text{m}^3}{\text{kg dry air}}} = 32.2 \frac{\text{kg dry air}}{\text{minute}}$$

$$\frac{\text{line 1-3}}{\text{line 1-2}} = \frac{w_{a2}}{w_{a2} + w_{a1}} = \frac{32.2}{32.2 + 117.9} = 0.21$$

Therefore, length of line segment 1-3 is 0.21 times the length of line 1-2

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0.87 m³/kg d.a. 0.95 m³/kg d.a.

$$T_3 = 40.0$$
°C
 $T_{w3} = 35.6$ °C